

Operational models for ice crystal formation in highly concentrated systems

E. López-Quiroga, P.J. Fryer, O. Gouseti, R. Wang and S. Bakalis
School of Chemical Engineering, University of Birmingham, UK.

Crystallisation

- ✓ important in food processing **freezing & freeze-drying**
- ✓ determining in creating microstructure (**food properties and texture**)
- ✓ challenging in **high concentrated systems** **available water?**

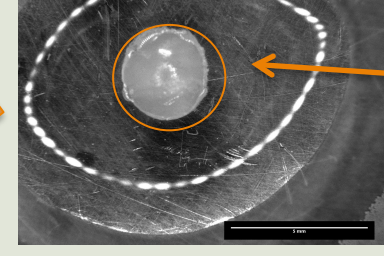
Why high concentrated systems?

Less water → Less energy consumption

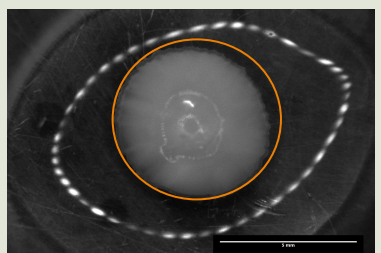
Experimental work

60% sucrose solution

Two crystallisation mechanisms

- **Secondary**


Seed



Growth
- **Primary homogenous**
Differential Scanning Calorimetry (DSC):
crystal fraction α

Secondary (seeding) model [1]

- Governing equations

$$\frac{\partial c_i}{\partial t} = \nabla(D_i \nabla c_i), \quad i = l, s$$

$$\rho_i C_{p_i} \frac{\partial T_i}{\partial t} = \nabla(k_i \nabla T_i), \quad i = l, s$$

- Moving front boundary conditions

$$\left[c |_{S(t)^+} - c |_{S(t)^-} \right] \frac{\partial S}{\partial t} = D_l \left. \frac{\partial c}{\partial x} \right|_{S(t)^+} - D_s \left. \frac{\partial c}{\partial x} \right|_{S(t)^-}$$

$$\Delta H \rho_s \frac{\partial S}{\partial t} = -k_l \left. \frac{\partial T}{\partial x} \right|_{S(t)^+} + k_s \left. \frac{\partial T}{\partial x} \right|_{S(t)^-}; T_i(S(t), t) = T_f^* - \Delta T$$

Freezing depression [3]

- External boundary conditions

$$T_s(0, t) = T_c < T_i(S(t), t); \quad \frac{\partial T_l}{\partial r}(R, t) = 0$$

$$c_s(0, t) = c_{seed}; \quad \frac{\partial c_l}{\partial r}(R, t) = 0$$

Homogeneous crystallisation model [2]

- Governing equations

$$\rho_m C_{p_m} \frac{\partial T_m}{\partial t} = \nabla(k_m \nabla T_m) + \rho_s \Delta H \frac{\partial \alpha}{\partial t}$$

- External boundary conditions

$$T_s(0, t) = T_c < T_i(S(t), t); \quad \frac{\partial T_l}{\partial r}(L, t) = 0$$

- Continuous material properties

$$k_m = \varepsilon k_{air} + (1 - \varepsilon)(\alpha k_s + [1 - \alpha] k_l)$$

$$C_{p_m} = \varepsilon C_{p_{air}} + (1 - \varepsilon)(\alpha C_{p_s} + [1 - \alpha] C_{p_l})$$

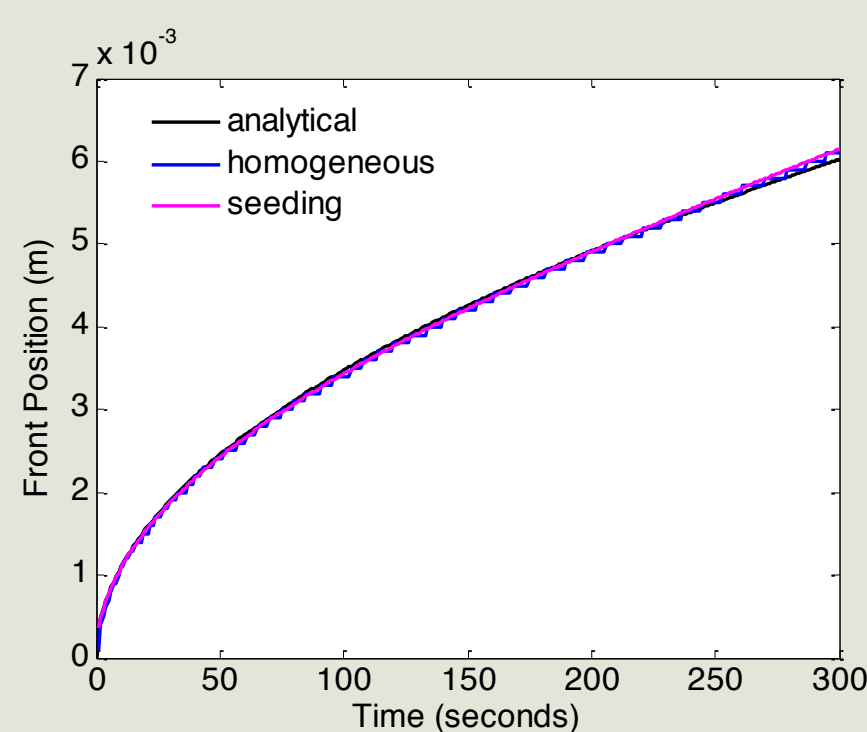
$$\rho_m = \varepsilon \rho_{air} + (1 - \varepsilon)(\alpha \rho_s + [1 - \alpha] \rho_l)$$

Crystal fraction

Numerical methodology & Results

Model validation

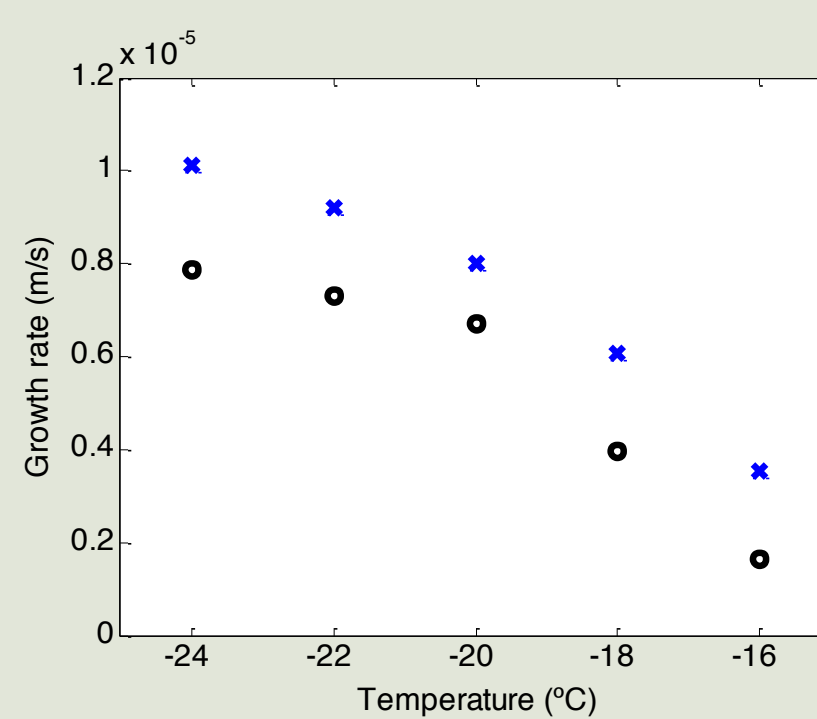
- Pure water, thermal problem
- Seeding: FEM+ALE (adaptive mesh)
- Homogeneous: FEM
- 101 nodes, tol=10⁻⁶



Comparison of the freezing front position evolution in time between the analytical and the proposed models solutions

Seeding results

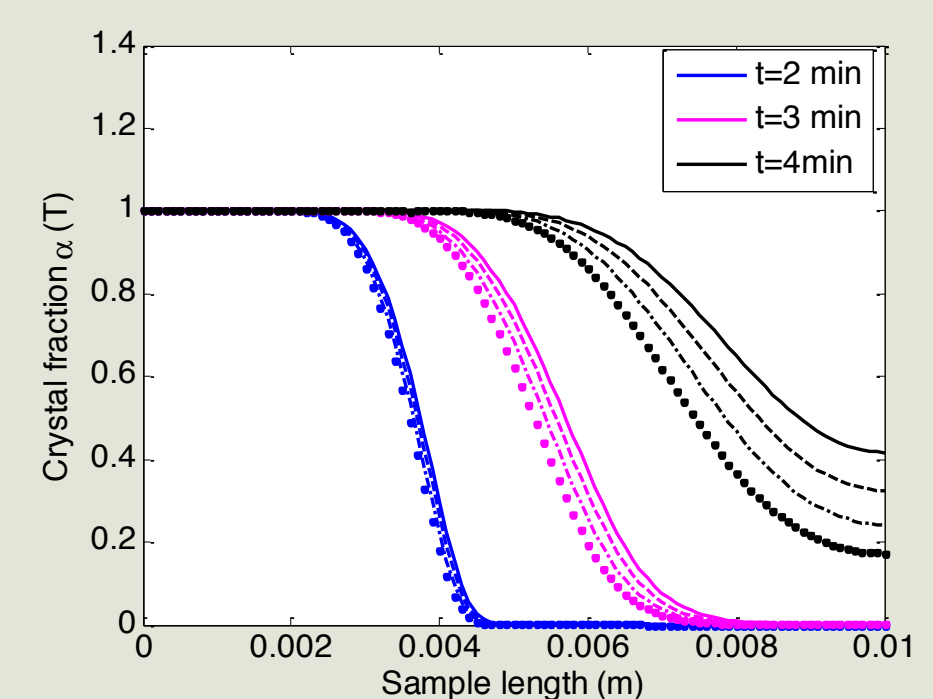
- 60% sucrose solution
- FEM+ALE (adaptive mesh) in COMSOL
- 101 nodes, tol=10⁻⁶, R=1 cm



Comparison of experimental (o) and simulated (x) growth crystal rates for different cooling conditions

Homogeneous crystallisation results

- 60% sucrose solution
- FEM in COMSOL
- 101 nodes, tol=10⁻⁶, L= 1cm
- Air fraction $\varepsilon = [0, 0.1, 0.2, 0.3]$



Comparison of the crystal fraction along the sample between the non-aerated 60% w/w sucrose solution (solid), and the aerated solution with air fractions (dashed), (dashed-dot) and (dot)

Conclusions

- Overall good agreement between models and experiments.
- Seeding model overestimates growth rates.
- Aeration affects heat transfer delaying ice crystal formation.
- Satisfactory first approach to modelling of high concentrated systems.

Acknowledgements

The authors acknowledge financial support received from EPSRC (grant no. EP/K011820/1).

REFERENCES

- [1] *Free and moving boundary problems* (1984), Clarendon Press, Oxford, UK.
- [2] *International Journal of Refrigeration* (2010) **33**, 1559-1568.
- [3] *Phase transitions in foods* (1995). Academic Press, London.